



## ABSTRACT

*Preliminary design of ethylene plant from propane is intended to assess the feasibility of the plant. This plant is designed to with a capacity of 600.000 tons per-year and operated continuously for 330 days per-year and 24 hours per-day.*

*This ethylene plant consists of 3 main processes, thermal cracking, H<sub>2</sub>O and H<sub>2</sub> removing, separation and product refining. Production of ethylene is carried out in furnace reactor using high temperature thermal cracking of propane. Then, product is refined and separated from by-products such as hydrogen, methane, propylene, and benzene to obtain 99.9% of ethylene purity.*

*This plant is planned to be established in Cilegon, Banten, with consideration of the raw materials transportation and product distribution. This plant requires 40.000 m<sup>3</sup> area with 300 employees.*

*Based on the criteria, this plant is classified as high-risk plant. In order to run the production process, fixed capital required amounted to \$ 100.188.747,93 + Rp. 203.732.436.556,47 and working capital required amounted to \$ 320.678.127,17 + Rp. 11.572.691.667,66. Total production cost required amounted to \$ 971.281.093,03 + Rp. 83.703.852.061,99. Profit before taxes per annual amounted to Rp. 741.941.154.322,65, while profit after taxes is Rp.556.455.865.741,99. Economic analysis result shows that Return on Investment (ROI) before taxes is 46,36% and ROI after taxes is 34,77%; Pay Out Time (POT) before taxes is 1,73 years and POT after taxes is 2,17 years; Break Even Point (BEP) is 48,67% of production capacity, Shut Down Point (SDP) is 35,93% of production capacity, Discounted Cash Flow Rate of Return (DCFRR) is 18,26%. From those points it can be concluded that preliminary design of this ethylene plant is appealing to be further assessed.*

**Keywords:** *Ethylene, Propane, Thermal Cracking*